

Final report

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*The guidance text (in italic) should be deleted, so the application form **only** contains numbered headings as well as relevant text from the applicant.*

1. Project details

Project title	SpeedUp
File no.	64020-1021
Name of the funding scheme	Energieffektivitet
Project managing company / institution	Weel & Sandvig
CVR number (central business register)	27255817
Project partners	Eceryg AB, DTU-MEKANIK
Submission date	13 March 2023

2. Summary

2.1 In English

The overall goal of the project is to develop an economically attractive heat pump for efficient electrification of the industry's energy consumption with a view to reducing the emission of greenhouse gases. The primary market segment is heat pumping in the temperature range 80 to 200°C and in the heat output range ½-5 MW with unit sizes of heat pumps in the range ½-1 MW heat.

The project partner Eceryg has developed a prototype unit (full scale) of a high speed motor directly coupled to a turbo compressor. The unit was first tested in air, where challenges with vibrations and rotor dynamics caused delays in the project. Different solutions were tested and through experience gained here, this challenge was finally handled in a satisfactory manner.

The unit was then thoroughly tested with water vapor as the working medium in a test rig built for the purpose. The compressor performances (flow at varying pressure conditions), efficiencies and various losses in auxiliary equipment are either measured or calculated. The experiments have shown stable operation with high efficiency, which is very promising for the future perspective of the technology and the prototype device.

The successful development and testing means that we are now preparing the next phase towards market maturation of the technology through an industrial demonstration, also on a full scale. In fact we have already received a commitment from an industrial host willing to participate in a full scale industrial long term demonstration project.

2.2 In Danish

Projektets overordnede mål er at udvikle en økonomisk attraktiv varmepumpe til effektiv elektrificering af industriens energiforbrug med henblik på at nedbringe udledningen af drivhusgasser. Markedssegmentet er varmepumpning i temperaturområdet 80 til 200°C og i varmeeffektområdet ½-5 MW med enhedsstørrelser på varmepumper i området ½-1 MW varme.

I projektet er udviklet en prototype-enhed (i fuld skala) af en højhastighedsmotor direkte sammenkoblet med en turbokompressor. Enheden er først testet i luft, hvor udfordringer med vibrationer og rotordynamik gav anledning til forsinkelser i projektet. Forskellige løsninger blev afprøvet og med erfaringer opnået herigennem er denne udfordring håndteret på tilfredstillende måde.

Enheden er derefter grundigt testet med vanddamp som arbejdsmedium i en testrig opbygget til formålet. I riggen er målt kompressorydelser (flow ved varierende trykforhold), virkningsgrader og beregning af diverse tab i hjælpeudstyr. Forsøgene har vist stabil drift med høj effektivitet, som er lovende for det fremtidige perspektiv for teknologien.

Den succesfulde udvikling og afprøvning betyder at vi nu er i gang med at forberede næste fase frem mod markedsmodning af prototypen gennem en industriel demonstration. Vi har således fået tilsagn fra en industriel partner, som har givet tilsagn til at deltage i et projekt (forudsat at der opnås finansiel støtte) hvor planen er at teknologien skal igennem industriel langtidsdemonstration i fuldskala.

3. Project objectives

The objective is to develop a cost effective and efficient high temperature heat pump suited for implementation in industrial processes. The purpose of the heat pump is to upgrade excess heat available in certain processes for substituting existing steam generation based on combustion of fuels in traditional boilers with related CO₂ emission. The heat pump is powered by a high speed electrical motor, where related emission of green house gases in the electricity consumption is already very low and expected still decreasing.

The technology is based on combining a very high speed electrical drive (motor and frequency converter) in a direct coupling with a small turbo compressor in order to achieve a suitable and cheap steam compressor unit for compressing steam (clean water vapour) in a capacity range that fits with the demand and temperature requirements in many industrial sites.

A full scale steam compressor unit of this most advantageous technology has been developed and demonstrated successfully in the project in a specially developed test rig installed at DTU lab. facility.

In order to achieve a suitable and efficient turbo compressor for the targeted capacity and temperature levels the rotations speed needs to be higher than 50000 rpm. The electric motor has a power capacity of 110 kW at 70000 rpm. This is close to the technical limits (see Figure 1).

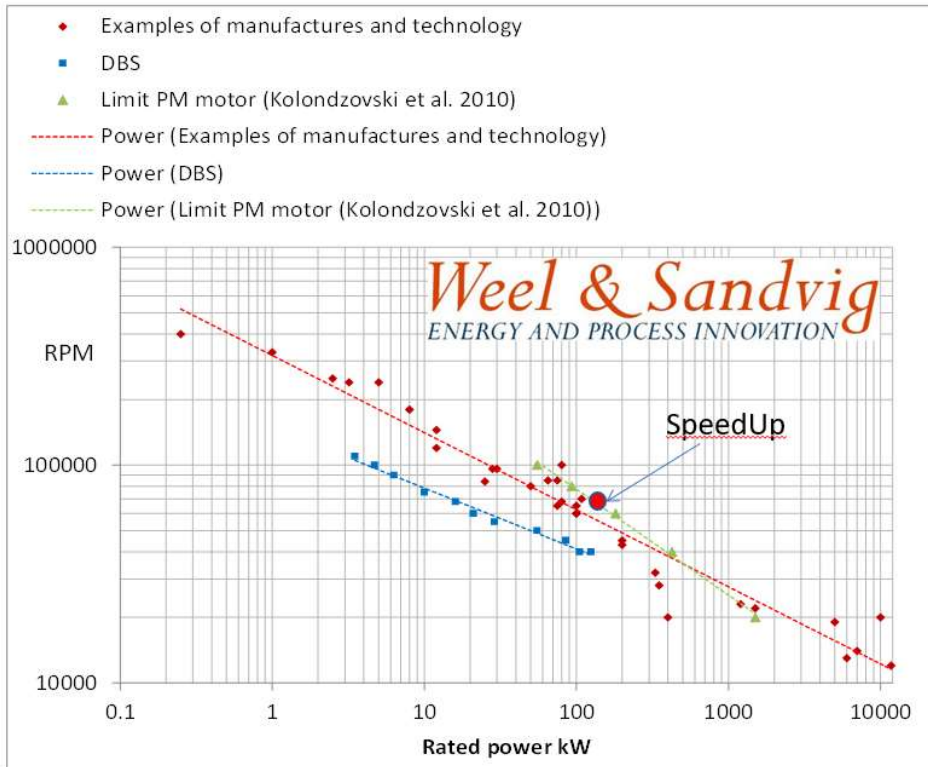


Figure 1. Relation between shaft power and maximum speed for electric motors.

4. Project implementation

The development of the prototype unit began with extensive investigation of the design and performance evaluation of a high speed turbo compressor unit combined with a high speed rotor design and sealing system.

Performance of the compressor operating in steam is investigated by Weel & Sandvig and MEK, DTU (Brice, post doc) by use of CFD-modeling and simulation. Brice used The “Frozen rotor” method combined with exploiting axial symmetries (impeller is with splitter meaning two channels are included) was used for reducing the size of the model. ANSYS CFX was chosen for the study due to its high performances in turbomachinery applications.

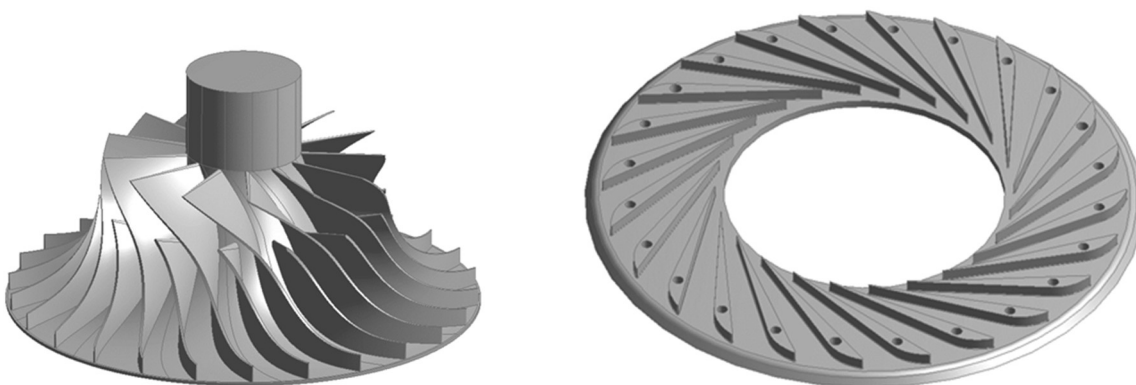


Figure 2. 3-D model of the impeller (left) and the diffuser (right).

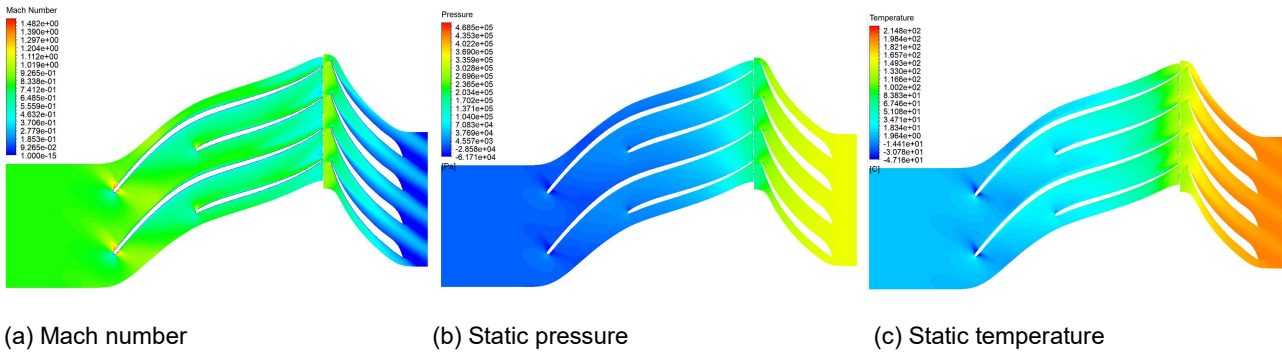
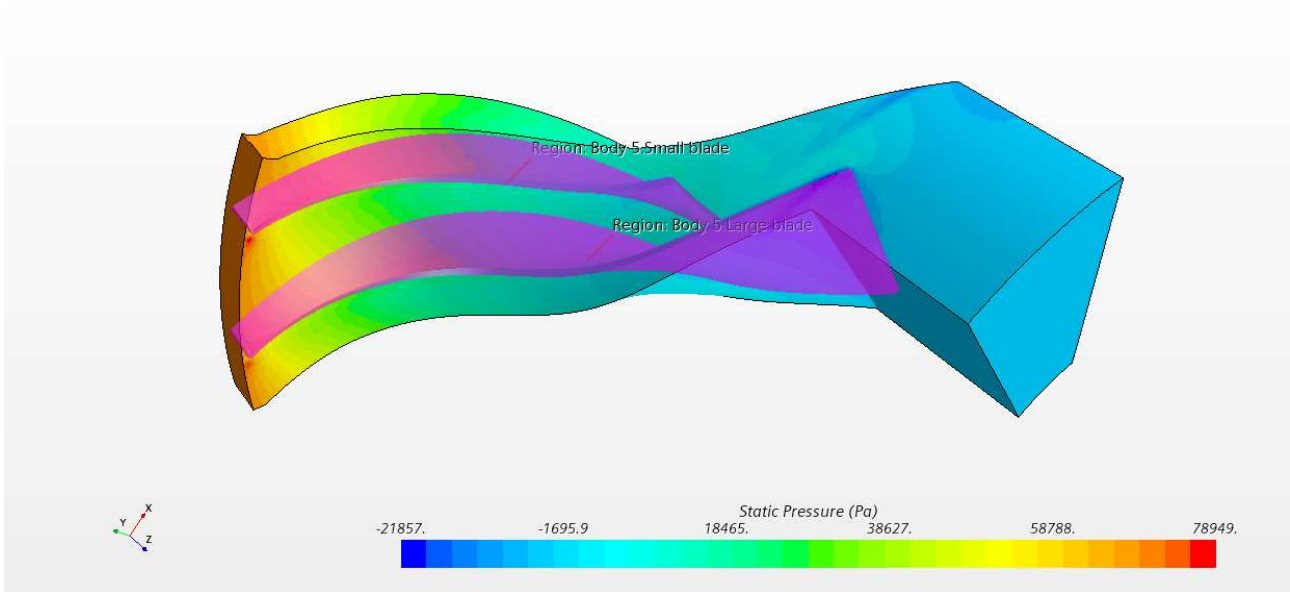


Figure 3. Compressor performance (Ansys CFX in air) for $\omega=66500$ RPM, $PR=4.35$, $m=0.856$ and $\eta=0.850$, $Span=0.5$.



Figur 1 3-D view of static gauge pressure through impeller segment with steam at 70000 RPM. Impeller static outlet pressure =0.7 barg and total pressure = 1.48 barg (inlet total pressure 0 barg and 388 K).

Extensive and numerous investigations and modifications of rotor design was applied before suitable rotor dynamics, vibrations levels and restricted speed range due to critical speed was achieved. This part of the project was more tedious and time consuming than expected. Though, due to our experiences achieved, we expect that possible limitations on other future rotor designs for specific applications (capacity, temperature levels and temperature lifts) will not be a major problem or imply serious limitations concerning operational range and restrictions related to critical speed ranges.

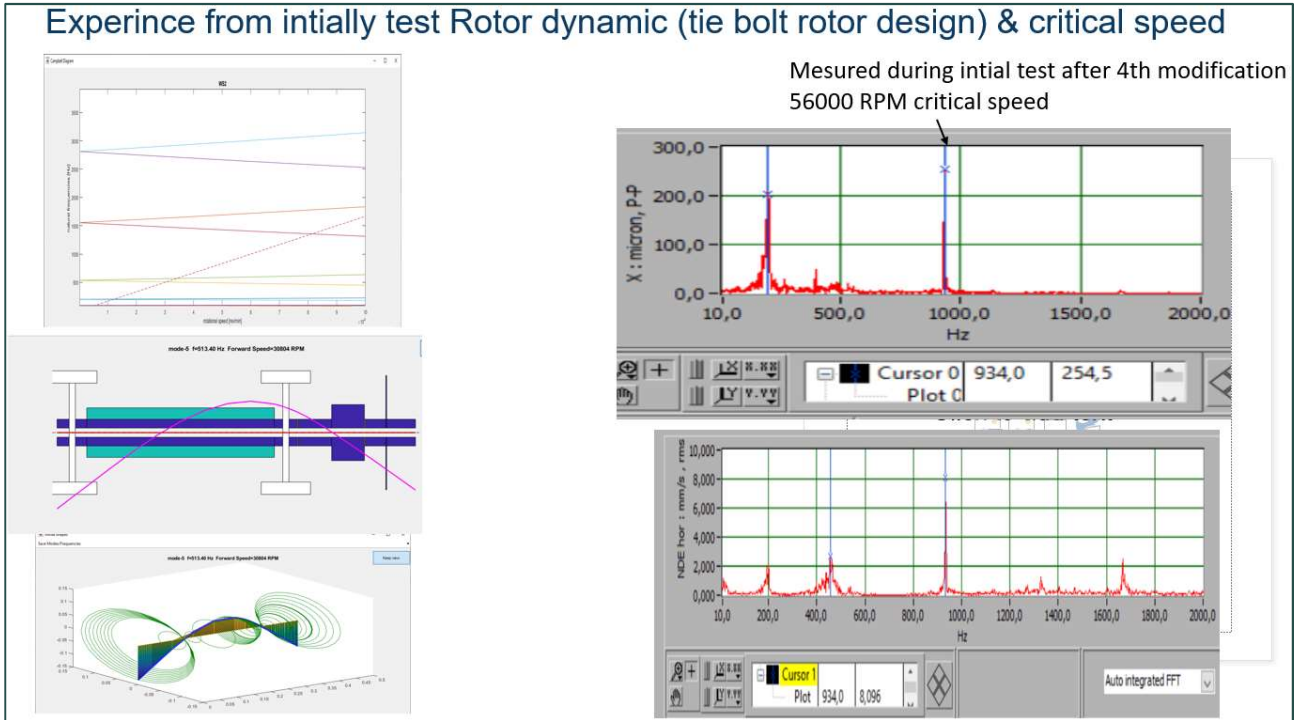


Figure 4. Left: Analysis of rotor dynamics. Right: Vibration analysis applied by Colding A/S.

In parallel to the development of the steam compressor a test rig suitable of testing and measuring performance of the compressor operating in steam was designed and erected in a lab facility at DTU.

The compressor unit has been tested in numerous operating points in steam and the performance has been measured.

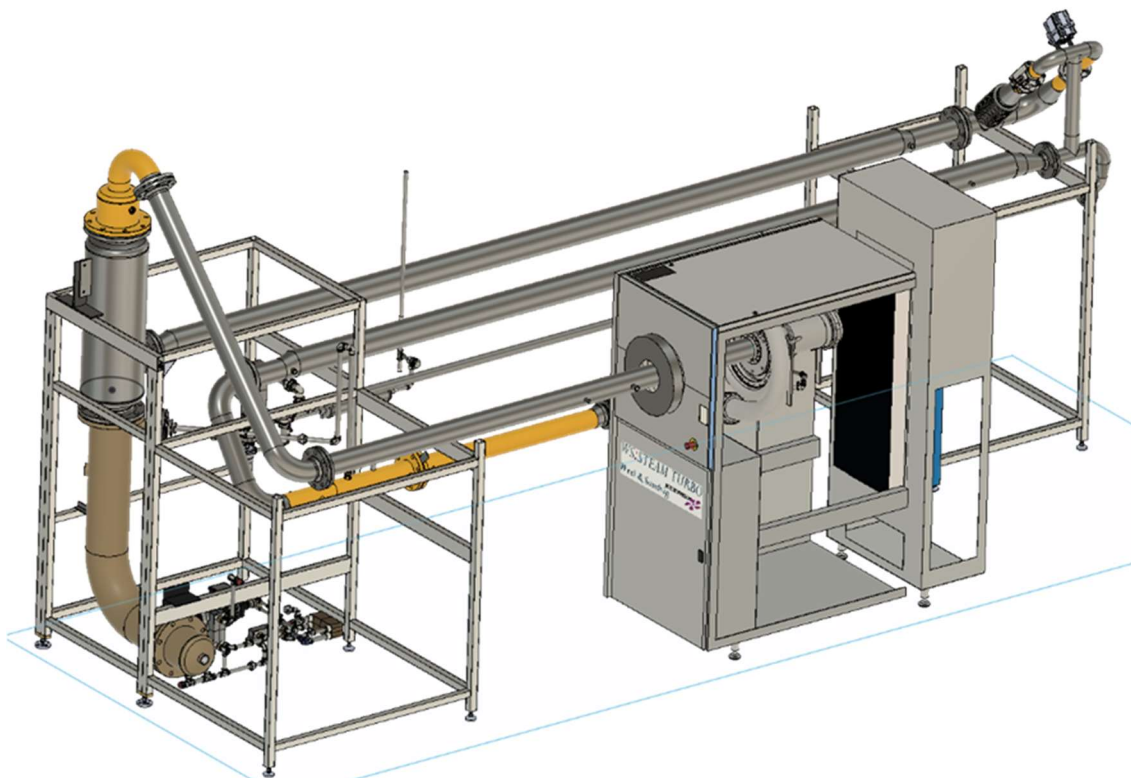


Figure 5. Design of test rig (Weel & Sandvig).



Figure 6. Left: Test rig and compressor unit as built and installed at DTU lab. Lower right: turbo compressor impeller (outer diameter 142 mm) capable of delivering 1 MW condensing heat at 133 C with a temperature lift of 25 C at a rotational speed of 70000 rpm. Upper right: For comparison of impeller size: the size of a normal beverage can.

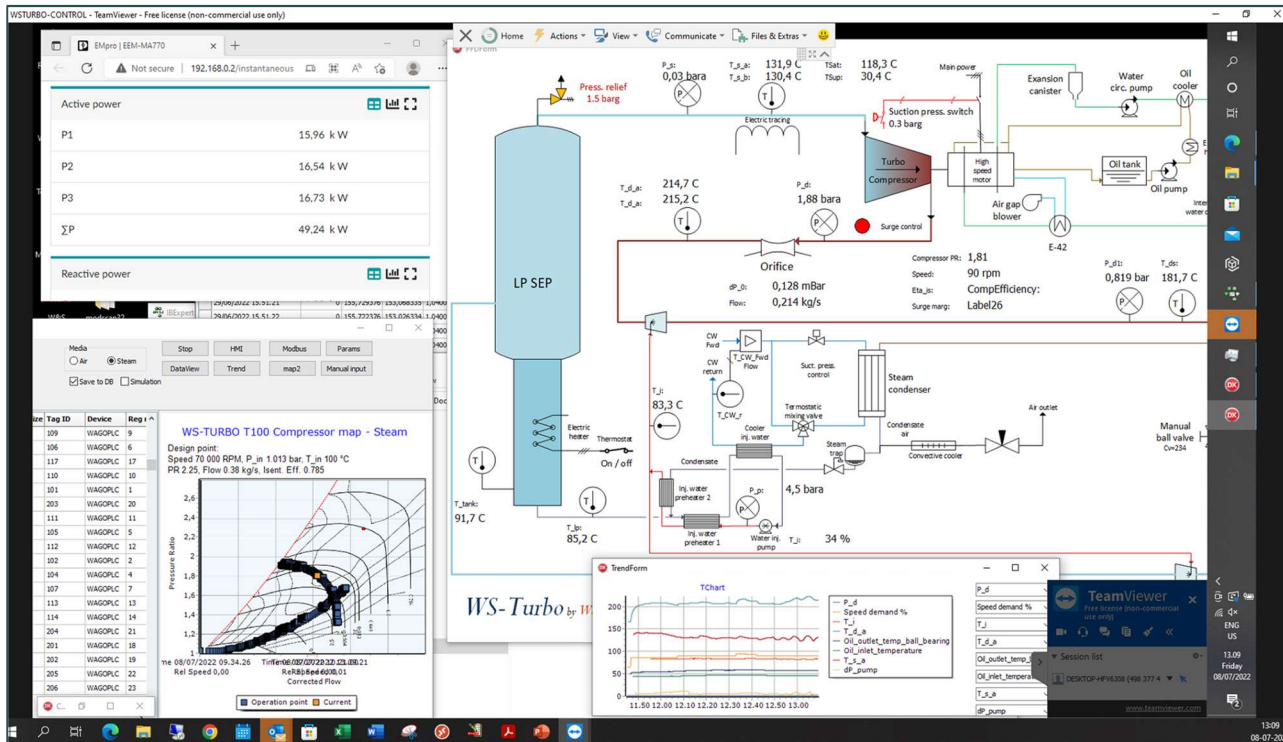


Figure 7. Screen from performance and data acquisition system (WS-Turbo).

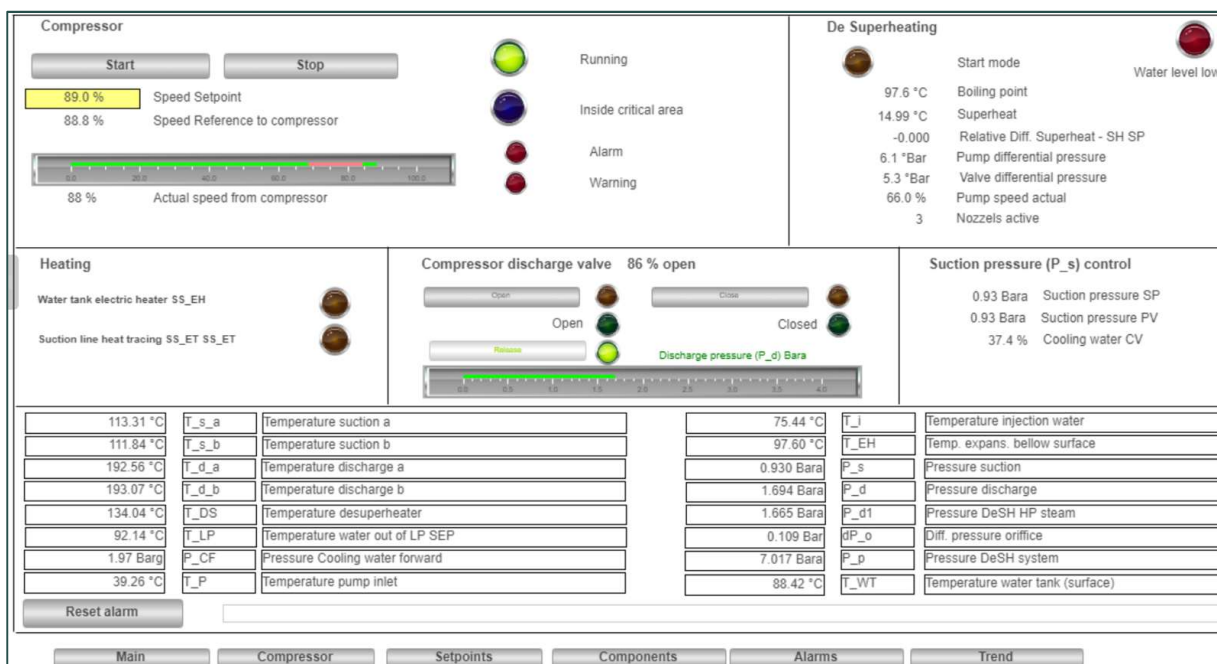


Figure 8. "Main" screen of the test rig control system.

Compressor

Start **Stop**

89.0 % Speed Setpoint
88.8 % Speed Reference to compressor



88 % Actual speed

49.0 °C Oil inlet temperature
61.1 °C Oil outlet temperature ball bearing
59.6 °C Oil outlet temperature roller bearing
27.8 °C Buffer air temp inlet
69.5 °C Buffer air temp outlet
27.2 °C Cooling water temp
57.1 °C Generator coil temp
41.3 °C Enclosure temp
-0.2 g Vibrations
17 Passes in critical area

Actual Speed	101 %	trip level	warning level
Oil inlet temperature	70 °C	65 °C	65 °C
Oil inlet temp Ball bearing	90 °C	85 °C	85 °C
Oil outlet temp Roller bearing	90 °C	85 °C	85 °C
Buffer air temp inlet	65 °C	95 °C	95 °C
Buffer air temp outlet	105 °C	95 °C	95 °C
Cooling water temp	80 °C	100 °C	100 °C
Generator coil temp	105 °C	100 °C	100 °C
Vibration	18 g		
Enclosure temp	65 °C		

Running 2115 Minutes
1255 Minutes * relative speed
795 Minutes * (relative speed to the power of 3)

Inside critical area

- Alarm
- Warning
- Emergency button pressed
- Buffer air fault during start
- Oil pressure fault during start
- Oil pre heat fault during start
- Sensor fail buffer air pressure switch
- Sensor fail oil pressure switch
- Speed_not_detected_during_start
- BMS heart stop
- Auxiliary system fault
- Roll out fault
- Overspeed fault


- Oil_inlet_temperature_low
- Oil_inlet_temperature_high
- Oil_outlet_Roll_bearing_temperature_high
- Oil_outlet_Ball_bearing_temperature_high
- Oil_level_low_in_tank
- Oil_pressure_low
- Buffer_air_pressure_low
- Buffer_air_inlet_temperature_high
- Buffer_air_outlet_temperature_high
- Cool_water_temperature_high
- Vibration_high
- Generator_coil_temperature_high
- Speed too low during running
- inverter unit fail
- Enclosure temp switch

Reset compressor fault

Main
Compressor
Setpoints
Components
Alarms
Trend

2.5 bar	Min_dp_set	Minimum difference pressure pump setpoint
11.0 bar	Max_dp_set	Maximum difference pressure pump setpoint
25 °C	SH_set	Super heating setpoint
25 °C	SH_set_start	Super heating starting setpoint
50 °C	SH_Range	Super heating range for De superheat pump controller
0.100	SH_acc	Super heating relative deviation limit to start De superheating
<small>Normal set point (°C)</small>		
8.50	S_p_min	Min de-superheat pump speed
<small>Normal set point (°C)</small>		
20 sec	NZ_L_1	Time between 2 consecutive closing of nozzles
20 sec	NZ_L_2	Time between 2 consecutive opening of nozzles
20 °C	Min_T_s_start	Minimum temperature before start of compressor
20.0 °C	PT_set	addition to calculated saturation temperature
35 °C	WT_set_start	Minimum temperature in water tank before start
1.0 bar	P_s_set_start	Minimum pressure in suction pipe before start
4.0 %/sec	C_ramp_up	Ramp for increasing compressor speed
4.0 %/sec	C_ramp_down	Ramp for decreasing compressor speed
0.93 bar	CW_p_set	Suction pressure (P_s) setpoint (cooling water control valve)
20 sec	CW_ds	Delayed closing of CW valve after compressor stop
1.013 bar	Atm_press	Atmospheric pressure
149 °C	T_EH_max	Suction line heat tracing interlock limit
136 °C	T_EH_set	Suction line heat tracing setpoint
56 °C	T_p_WL	Warning limit water pump inlet temperature
66 °C	T_p_AL	Alarm limit water pump inlet temperature
10.0 %/sec	C_ramp_critical	Ramp in the critical area
68.6 %	C_critical_low	Compressor critical speed lower limit
84.3 %	C_critical_up	Compressor critical speed upper limit
0.1 sec	PC_pulse	Pressure control valve pulse length


Main
Compressor
Setpoints
Components
Alarms
Trend

Valve NZ1a 

Mode: Manual

Auto **Manual**


Open **Close**

Valve NZ1b 

Mode: Manual

Auto **Manual**


Open **Close**

Valve NZ2a 

Mode: Auto

Auto **Manual**

Open **Close**

Pump SS_p 

Mode: Auto

Auto **Manual**

Start **Stop**


Manual setpoint: **65.0 %**

Actual speed: **58.0 %**

kp: **-1.0**

tau: **30 sec**


td: **0 sec**

Water tank electric heater SS_EH 

Mode: Auto

Auto **Manual**

Enable **Disable**

Suction line Heat tracing SS_ET 

Mode: Auto

Auto **Manual**

On **Off**

Cooling water PID

Mode: Auto

Auto **Manual**

max SP: **18.0 %**

CV: **39.9 %**

kp: **-20.0**

tau: **30 sec**

td: **0 sec**

Main
Compressor
Setpoints
Components
Alarms
Trend

Figure 9. Other screens from the test rig control system.

5. Project results

The original objective of the project is obtained. We have applied numerous test of the compressor unit compressing steam in a test rig constructed in the project. Performance measurements of the compressor unit and quantification of power and heat losses related to the utility system in terms of oil, water and buffer air systems have been conducted.

The results show a bit lower efficiency than expected, which among others may be related to larger clearances between impeller and compressor shroud than designed for and strictly necessary. During the testing phase in critical speed range possibly there has been more situations with rubs. Also, the impeller has been balanced several times, including removing smaller parts of some impeller blades at the inlet.

	Time	Speed %	T_s_avg °C	T_d_avg °C	P_s_avg bara	P_d_avg bara	PR_avg	dp_o bar	IF97 Gas constant R 461.5						
									T_s_sat °C	T_d_sat °C	h_s kJ/kg	S_s kJ/kgC	h_is_d kJ/kg	h_d_sat kJ/kg	h_d kJ/kg
1	06/10/2022 10.02.30	0.598	113.1	154.7	0.932	1.282	1.376	0.055	97.65	106.70	2703.4	7.466	2761.7	447.4	2784.0
2	06/10/2022 10.40.30	0.878	112.0	190.6	0.910	1.640	1.802	0.103	96.99	114.05	2701.4	7.472	2812.6	478.5	2853.7
3	06/10/2022 11.06.30	0.940	112.0	203.3	0.910	1.792	1.969	0.119	96.99	116.77	2701.4	7.472	2830.7	490.1	2878.3
4	06/10/2022 11.28.30	0.940	111.9	205.7	0.910	1.832	2.014	0.102	96.99	117.46	2701.1	7.471	2835.0	493.0	2883.1
5	06/10/2022 11.52.30	0.940	112.1	211.2	0.910	1.877	2.063	0.071	97.00	118.22	2701.6	7.472	2840.5	496.2	2893.7
6	06/10/2022 12.09.30	0.940	112.1	216.1	0.911	1.886	2.071	0.050	97.02	118.37	2701.6	7.472	2841.3	496.9	2903.6
7	06/10/2022 12.37.30	0.940	111.0	202.9	0.880	1.729	1.965	0.119	96.07	115.67	2699.7	7.483	2828.2	485.4	2877.9
8	06/10/2022 12.58.30	0.940	115.7	207.3	0.930	1.832	1.970	0.127	97.59	117.46	2708.7	7.480	2839.2	493.0	2886.1
9	06/10/2022 13.12.30	0.940	114.4	204.5	0.930	1.793	1.929	0.141	97.58	116.80	2706.1	7.474	2831.9	490.2	2880.9
10	06/10/2022 13.18.30	0.940	115.4	204.1	0.931	1.744	1.873	0.156	97.62	115.93	2708.0	7.478	2828.1	486.5	2880.3
11	06/10/2022 13.29.30	0.940	116.0	203.0	0.930	1.647	1.771	0.178	97.59	114.17	2709.3	7.482	2818.0	479.0	2878.5
12	06/10/2022 13.42.30	0.940	115.0	201.7	0.932	1.649	1.770	0.180	97.64	114.21	2707.1	7.476	2815.5	479.2	2875.9
13	06/10/2022 14.17.30	0.940	112.0	205.6	0.910	1.820	1.999	0.109	96.99	117.25	2701.4	7.471	2833.8	492.1	2882.9
14	06/10/2022 09.48.00	0.598	116.9	156.5	0.947	1.212	1.279	0.087	98.10	105.06	2710.8	7.477	2755.9	440.5	2788.1
15	06/10/2022 10.16.30	0.598	115.2	152.4	0.969	1.298	1.340	0.050	98.73	107.07	2707.3	7.458	2760.9	448.9	2779.1
16	06/10/2022 11.34.30	0.940	112.1	206.6	0.910	1.843	2.025	0.098	96.99	117.65	2701.5	7.472	2836.7	493.8	2884.9
17	06/10/2022 11.43.30	0.940	112.0	209.0	0.910	1.867	2.051	0.081	97.00	118.05	2701.5	7.472	2839.2	495.5	2889.4
18	06/10/2022 13.22.45	0.940	115.9	203.7	0.930	1.700	1.827	0.167	97.60	115.15	2709.1	7.481	2824.2	483.2	2879.7

	Time	Eta_is	T_lift °C	MVR	Mass flow kg/s	Gaspower kW	Q_cond. kW	COP gas power	COP_gp*T-lift °C	Heat/Power		
										Q_c/EmPro COP	COP Carnot	Eta Carnot
1	06/10/2022 10.02.30	0.724	9.1		0.140	11.29	327.1	28.98	262.4		42.0	
2	06/10/2022 10.40.30	0.730	17.1		0.207	31.56	492.3	15.60	266.1		22.7	
3	06/10/2022 11.06.30	0.731	19.8		0.230	40.64	548.8	13.50	267.1	10.6	19.7	53.7%
4	06/10/2022 11.28.30	0.735	20.5		0.215	39.16	514.3	13.14	268.9	10.2	19.1	53.4%
5	06/10/2022 11.52.30	0.723	21.2		0.182	35.04	437.2	12.48	264.9	9.4	18.4	50.8%
6	06/10/2022 12.09.30	0.692	21.4		0.154	31.07	370.0	11.91	254.3	8.6	18.3	46.7%
7	06/10/2022 12.37.30	0.721	19.6		0.226	40.19	539.8	13.43	263.2	10.6	19.8	53.5%
8	06/10/2022 12.58.30	0.736	19.9		0.238	42.30	570.4	13.49	267.9	10.8	19.7	54.7%
9	06/10/2022 13.12.30	0.720	19.2		0.248	43.42	593.8	13.68	262.8	11.0	20.3	54.1%
10	06/10/2022 13.18.30	0.697	18.3		0.257	44.20	614.4	13.90	254.5	11.3	21.2	53.1%
11	06/10/2022 13.29.30	0.643	16.6		0.265	44.88	636.4	14.18	235.2	11.5	23.4	49.2%
12	06/10/2022 13.42.30	0.642	16.6		0.267	45.12	640.9	14.21	235.4	11.5	23.4	49.2%
13	06/10/2022 14.17.30	0.729	20.3		0.222	40.21	529.7	13.17	266.8	10.4	19.3	54.0%
14	06/10/2022 09.48.00	0.583	7.0		0.169	13.10	397.9	30.37	211.4			
15	06/10/2022 10.16.30	0.747	8.3		0.136	9.74	315.8	32.44	270.5			
16	06/10/2022 11.34.30	0.737	20.7		0.212	38.80	506.0	13.04	269.4			
17	06/10/2022 11.43.30	0.733	21.0		0.194	36.47	464.6	12.74	268.1			
18	06/10/2022 13.22.45	0.675	17.5		0.262	44.63	627.1	14.05	246.5			

Figure 10. Performance data of compressor operation (6.th of October 2022).

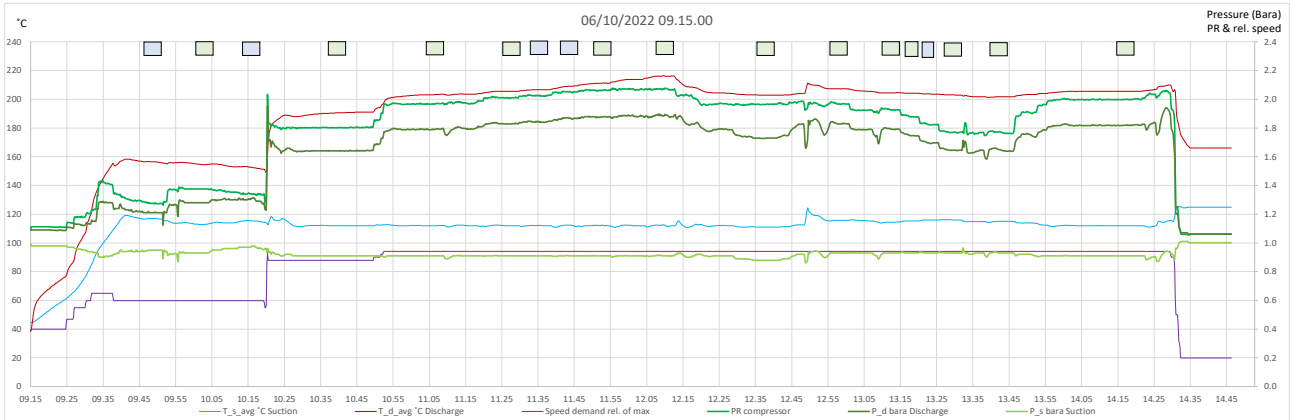


Figure 11. Example of compressor operation during a test (6.th of October 2022).

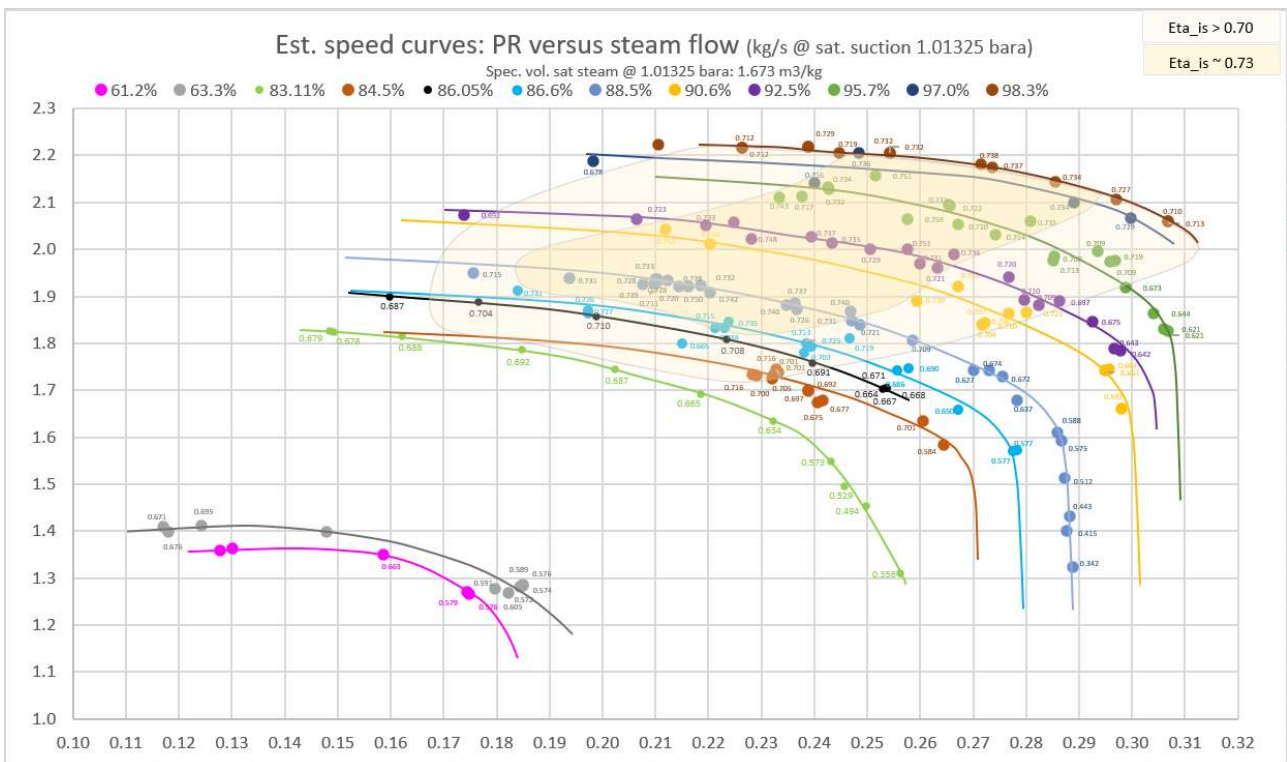


Figure 12. Compressor map based on measured performances in the Weel & Sandvig test rig.

In the project so far the compressor unit have demonstrated:

- About 120 hours of operation with steam.
- Inlet pressure from 0.6 bara to 1.3 bara.
- Steam suction capacity 0.2 – 0.6 m³/s (100 % speed).
- Inlet temperature from 90 C to 170 C.
- Pressure ratio 1.8 – 2.2 with actual test rig impeller design. New design up to 2.9 can be achieved.

- Discharge pressure demonstrated: 2.7 bara (130 C saturation temperature). Suction pressure was limited by power input and thereby also discharge pressure.
- Temperature lift 25 K in one stage providing a heat pumping COP of 8-10.
- Measured compressor isentropic efficiency 0.73 – 0.75.
- Loss in motor, inverter and aux system: Gas Power/Grid Power 0.82 at 80 % power.
- Very smooth and stable operation above 82 % speed (very low vibration level).
- Critical speed range (considered conservatively from 68 – 82 % speed) must be passed quickly.
- All safety systems for compressor startup and safe operation worked as expected.
- Slightly insufficient capacity of deSH and cooling for controlling the gas loop system at full load.
- Compressor system is on TRL 4-5 and is considered ready to test in real industrial environment.

6. Utilisation of project results

The project has demonstrated that the technology can work as efficient heat pumping in temperature and capacity ranges similar to many possible industrial applications, where existing heat pumping technology is either not suitable or applicable.

Industrial full scale demonstration on a long term is the next phase and the planning is started.

More competitors are developing heat pumps for high temperature heat supply (above 100 C). Large turbo compressors have for many years been available, but is not suitable for the smaller heat capacity range below 5 MW heat.

Traditional heat pump technologies is being redesigned for working at higher temperature levels. But we do not consider the traditional heat pumping technologies (based on mechanical displacement compressors) as a competitive technology for upgrading heat available at high temperatures.

7. Project conclusion and perspective

The project has successfully demonstrated a technology in full scale that delivers high temperature heat pumping with high efficiency suitable for upgrading excess heat to useful heat in industrial processes, and thereby reducing or eventually eliminating the demand for combustion of fuel related to steam generation in many industries.

The next step is to demonstrate operability and long term reliability in a real industrial site.

We certainly expect the technology will pass this real industrial demonstration phase successfully also, and thereby open the door for low-cost high-efficiency industrial heat pumping applications at high temperature levels. Thereby providing an important part of the industry a valuable, cost and resource efficient solution in the transition from fuel based heat supply to low emission electrified heat solution.

8. Appendices